

**GAS FORM C****Main particulars****2.1 PREAMBLE**

<b>Ship's name</b>	BW LIBERTY
<b>Owners</b>	BW Liberty Limited
<b>Flag – Registry</b>	Norway (NIS) - Oslo
<b>Builder</b>	Daewoo Shipbuilding & Marine Engineering Co. Ltd., Okpo, South Korea
<b>Delivery</b>	30 <sup>th</sup> November 2007
<b>Class</b>	Lloyd's Register
<b>Class notation</b>	+100A1, Liquefied Gas Carrier, Ship Type 2G, Butane, Propane, Anhydrous ammonia, in Independent Tanks Type A Maximum SG 0.69, Maximum Vapour Pressure 0.25 bar at sea(0.45 bar in harbour, Minimum Temperature -50° C, *IWS, LMC, IGS,UMS, NAV1, RMC(LG), ShipRight(LG), LI
<b>IMO No.</b>	9350288

<b>GRT / NRT</b>	
<b>International</b>	48,456 / 17,304
<b>Suez</b>	51,346.2 / 46,001.57
<b>Panama</b>	N/A

**2.2 HULL**

	<b>Metres</b>
<b>LOA</b>	226.00 mtrs
<b>LBP</b>	215.00 mtrs
<b>Breadth</b>	36.61 mtrs
<b>Depth</b>	22.20 mtrs
<b>Keel to highest point</b>	54.765 mtrs
<b>KTM (lowered antenna)</b>	52.365 mtrs

<b>Max summer draft</b>	11.822 mtrs	<b>Corresponding deadweight</b>	54,975 mt
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<b>TPC fully loaded</b>	70.87 mt
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<b>Mean draft with 95% full bunkers and full cargo</b>		
<b>Specific Gravity</b>	<b>Mean draft</b>	<b>Corresponding DW</b>
0.581 (C3 – 98%)	11.462 m	52,431
0.596 (C4 – 98%)	11.697 m	54,089
0.680 (NH3 – 87%)	11.822 m	54,975
0.703	N/A	N/A



<b>Communication equipment</b>	
<b>International call sign</b>	LAMM7
<b>Radio station</b>	GMDSS
<b>Satcom F-77</b>	
- Telephone	+870 765 065 045 / 46
- Telefax	765 065 047 / 48
<b>V Sat</b>	
- Telephone	+47 85 23 07 03 / +65 31 58 09 71
<b>Satcom C</b>	+870 425 907 110
<b>Cell phone</b>	+47 97 56 69 28
<b>MMSI</b>	259 071 000
<b>E-mail</b>	liberty@bwfleet.com

**2.3 MACHINERY**

<b>Main Engine</b>	
STX - MAN B & W 6S60 MC - C	
<b>Service power (90% MCR)</b>	12,200 kW at 101.4 RPM
<b>Grade fuel used</b>	HFO up to 600 cSt at 50C

<b>Auxiliaries</b>	
<b>Diesel</b>	3 units
<b>Make</b>	Yanmar 8N21AL-GV
<b>kW/RPM (100%)</b>	1,270 kW / 900 rpm
<b>Grade fuel used</b>	HFO up to 600 cSt at 50C / MDO grade ISO-F-DMB-DMA

<b>Speed/Consumption*</b>	
Guaranteed average loaded/ballast speed over 12 months	
Average consumption on Main Engine guaranteed speed	
Average consumption on auxiliaries	

\*) Above based on 50/50 propane/butane and max force 5 Beaufort

<b>Slow speed/consumption figures as guidance only</b>	
Average loaded/ballast	Consumption
13 Knots	
14 Knots	
15 Knots	

<b>Average consumption in port</b>	
<b>Inert gas plant when operating</b>	
<b>Boiler consumption</b>	

<b>Permanent bunkers capacity (98% full) (Incl. daily service and settling tanks)</b>	
<b>HFO</b>	3,390 mt
<b>Diesel Oil</b>	145 mt
<b>Light Diesel Oil</b>	95 mt



2.4 CARGO INSTALLATION

Transportable products and respective quantities								
Tank No.	100 % m <sup>3</sup>	98 % m <sup>3</sup>	n-Butane 0.602 -0.08°C mt	Propane 0.579 -42.12°C mt	Ammonia 0.682 -33.6°C mt			
1	18,412.55	18,044.30	10,737	10,362	10,816			
2	22,360.33	21,913.12	13,040	12,584	13,135			
3	22,349.96	21,902.96	13,034	12,578	13,129			
4	21,474.40	21,044.91	12,523	12,085	12,615			
<b>Total</b>	84,597.24	82,905.29	49,334	47,609	49,695			
<b>Deck tank capacity</b>					N/A			
Transportable products and respective quantities								
<i>Other transportable products:</i>								
<i>Propane with max 5 mole % Ethane in liquid phase / Mixture of Propane and Butane in any proportion</i>								

Scantlings of the cargo tanks are based on a maximum density of cargo of 610 kg/m <sup>3</sup> . Cargo with density up to 1,000 kg/m <sup>3</sup> may be carried in the cargo tanks on the following conditions:	
For density of 1,000 kg/m <sup>3</sup>	N/A
For densities between 610 and 1,000 kg/m <sup>3</sup>	87% by volume for cargo density of 690 kg/m <sup>3</sup>

Tank working pressure	
Maximum pressure	0.450 barg (harbour) / 0.250 barg (sea)
Minimum pressure	-0.050 bar
Minimum temperature acceptable in tanks	-50 °C

Loading rate - tons/hour	2,500 mt on two manifolds
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2.5 CARGO PUMPS

Number and type	8 x 600 m3/hr Hamworthy Svanehoj Centrifugal Deepwell pumps
Location	2 x pumps in each cargo tank
Max permissible specific gravity	120 mLC, 690 kg/m3
Time for discharging full cargo using all pumps against no backpressure	20 hrs
Cargo remaining onboard in cargo tanks after completion pumping	Total appr 60 m3 unpumpable liquid (all cargo tanks)
Total head when working in series with booster pump	235 mLC
Booster pumps	2 x 600 m3/h Hamworthy Svanehoj Centrifugal, 115 mLC, 690 kg/m3



2.6 CARGO COMPRESSORS

<b>Number and type</b>	4 x Sulzer Burckhardt piston Compressor 3K 140-3A		
<b>Refrigeration Capacity</b>	<b>Propane</b> 242 kW (5.0% Ethane)	<b>n-Butane</b> 345 kW	<b>Ammonia</b> 398 kW
<b>Suction pressure</b>	0.200 bar		

2.7 INERT GAS SYSTEM

<b>Does the vessel use inert gas?</b>	Yes
<b>Utilization</b>	Inerting of Void spaces and Cargo tanks

<b>Does the vessel produce inert gas?</b>	Yes
<b>Type</b>	Hamworthy Moss Inert Gas Generator
<b>Daily production</b>	120,000 m <sup>3</sup>

Composition of inert gas	
<b>Carbon dioxide</b>	14.0 %
<b>Oxygen max.</b>	1.0 %
<b>Carbon monoxide max.</b>	100 ppm by volume
<b>Hydrogen max.</b>	Nil
<b>Nitrogen</b>	Balance (84.9) %
<b>Soot</b>	Bacharach 0
<b>Sulphur oxides max.</b>	1 ppm by volume
<b>Dew point</b>	-45 °C at 760 mmHG

<b>State if any shore supply of liquid nitrogen may be required</b>	No
<b>What quantity?</b>	N/A

2.8 GAS FREEING

<b>Can this operation be carried out at sea?</b>	Yes
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<b>State method incl. all details</b>	
<b>For LPG</b>	<b>Boil Off</b> 18/24 hrs C3/C4
	<b>Inerting</b> 30 hrs
	<b>Ventilating for Entry</b> 30 hrs (IG blower)
<b>For NH<sub>3</sub></b>	8 days down to 50 ppm

<b>Advise time required and consumption of inert gas if any</b>	
<b>From LPG approximately</b>	30 hrs / 150,000 m <sup>3</sup>
<b>From NH<sub>3</sub> approximately</b>	N/A (venting with air)

<b>Is the vessel equipped with inert gas blower?</b>	Yes
<b>Capacity</b>	5,000 m <sup>3</sup> /hr

<b>Ventilation fan</b>	N/A (Inert gas blower to be used)
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**2.9 CHANGING GRADE**

Can this operation be carried out at sea?	Yes
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**State method used and time required for changing from NH<sub>3</sub> to LPG and vice versa, to reach 50 ppm of previous cargo in tanks atmosphere, the tanks being dry and free of moisture (dewpoint +10 degrees C)**

<b>From NH<sub>3</sub> to LPG</b>	Boil off, Heating up, Venting with air and Inerting
<b>Time required</b>	About 9.5 days

<b>From LPG to NH<sub>3</sub></b>	Boil off, Heating up, Inerting and Venting with air
<b>Time required</b>	About 4.5 days

<b>Can vessel reduce in tank atmosphere and gas installation concentration of previous cargo below 50 ppm?</b>	Yes
<b>Method used, time required and extra shore supply if any</b>	Boil off / heating / inerting / venting
<b>How can it be checked that no liquid gas remain onboard</b>	Level Gauge / Temperature sensors

**2.10 CARGO HEATER**

<b>State discharging rate for propane with 2.5 mol % ethane to be brought from -42 °C to 0 °C at sea temperature of 15 °C</b>	600 m <sup>3</sup> /hr
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**2.11 CARGO VAPORIZER**

<b>In case of need of vapour gas during discharge, can vessel produce its own if no shore gas available?</b>	Yes
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**2.12 REFRIGERATING APPARATUS**

<b>Is it independent of cargo?</b>	Yes
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**2.13 MEASURING APPARATUS**

<b>What gauges onboard</b>	Level gauges
<b>Location and type</b>	2 for each cargo tank / Radar type
<b>Number of temperature sensors/gauges pr tank</b>	7 – (3 each side of tank and 1 in vapour dome)
<b>Number of pressure sensors/gauges pr tank</b>	1 in each tank



2.14 SAMPLES

Where can samples be taken?	Vapour on dome / Liquid on dome using cargo pump and manifold
Are sample bottles available onboard?	No

2.15 CARGO LINES

(See also last page of this gas form C)

Is vessel fitted with midship manifolds	Yes
Distance from cargo manifold to bow	114.21 mtrs
Distance from manifold to stern	111.79 mtrs
Height cargo manifold above main deck	1.564 mtrs
Height cargo manifold above waterline when in ballast	16.300 mtrs
Height cargo manifold above waterline when loaded	11.970 mtrs
Distance from shipside to manifold flange	3.000 mtrs
Distance between loading and vapour return connections	2.50 mtrs
Windage area in normal ballast condition	4,080.6 m2
Is vessel fitted with SPM chainstopper suitable for 76 mm chain.	Yes
Is vessel fitted with cruciform bollards/fairleads/eye-pads in manifold area	Yes

Dimension of lines		
	Diameter	Flange size
Liquid System 1	400 mm / 16 inch	ANSI 300
Liquid System 2	400 mm / 16 inch	ANSI 300
Gas Line	250 mm / 10 inch	ANSI 150
Booster Line	350 mm / 14 inch	ANSI 300

What reducers onboard			
Number	Diameter	Length	Pressure rating
2	16" - 16"	50 cm	ANSI 300 - ANSI 300
2	16" - 12"	50 cm	ANSI 300 - ANSI 300
2	16" - 10"	50 cm	ANSI 300 - ANSI 300
2	16" - 8"	50 cm	ANSI 300 - ANSI 300
2	16" - 16"	50 cm	ANSI 300 - ANSI 150
2	16" - 14"	50 cm	ANSI 300 - ANSI 150
2	16" - 12"	50 cm	ANSI 300 - ANSI 150
2	16" - 10"	50 cm	ANSI 300 - ANSI 150
2	16" - 8"	50 cm	ANSI 300 - ANSI 150
2	10" - 12"	50 cm	ANSI 150 - ANSI 150
2	10" - 10"	50 cm	ANSI 150 - ANSI 150
2	10" - 8"	50 cm	ANSI 150 - ANSI 150
2	10" - 6"	50 cm	ANSI 150 - ANSI 150

2.16 LIFTING DEVICE

Where situated	Aft	Amidship
Number and type	2	1
Lifting capacity	4 tons	5 tons
Max. distance from ship's side of lifting hook	Port 4.0 mtrs Stb. 4.0 mtrs	8.5 mtrs

**2.17 HOSES**

<b>For what products are hoses suitable</b>	N/A
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<b>Number</b>	<b>Length</b>	<b>Diameter</b>	<b>Working pressure</b>	<b>Flange</b>
0	N/A	N/A	N/A	N/A

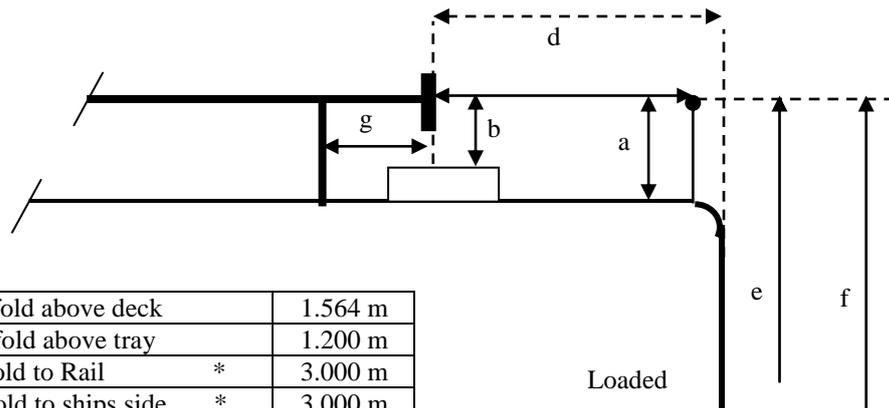
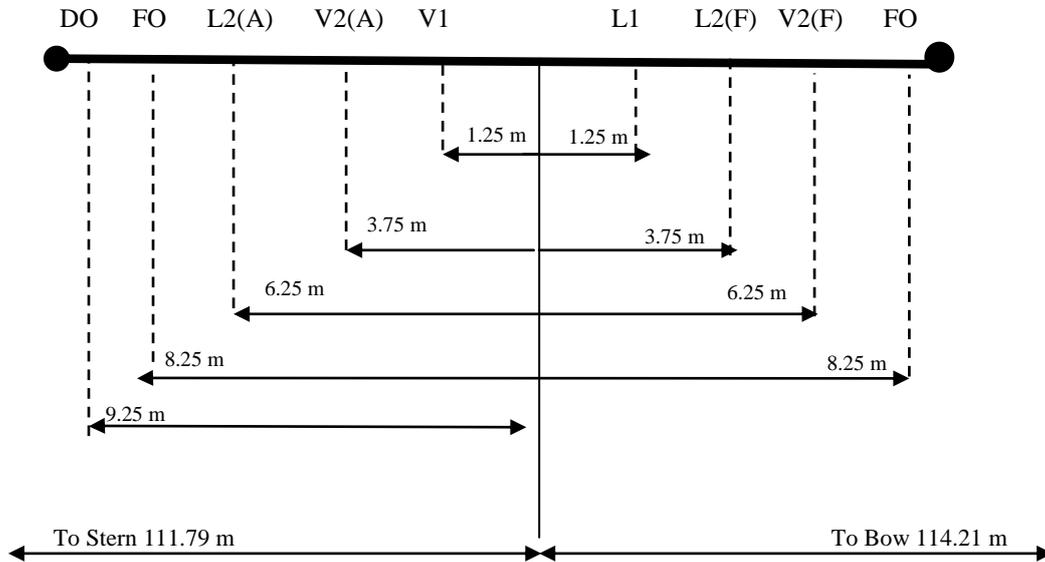
**2.18 SPECIAL FACILITIES**

<b>How many grades can vessel segregate?</b>	2
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<b>Indicate systems</b>	(Tks 1+3) and (Tks 2+4) or (Tks 1+3+4) and (Tk 2)
<b>Is vessel able to load/discharge two or more grades simultaneously?</b>	Yes
<b>Can vessel sail with slack tanks?</b>	Yes
<b>Is vessel fitted with purge tank?</b>	No



### ARRANGEMENT OF CARGO MANIFOLD



a) Height of manifold above deck	1.564 m
b) Height of manifold above tray	1.200 m
c) Distance manifold to Rail *	3.000 m
d) Distance manifold to ships side *	3.000 m
e) Dist. waterline loaded to manifold	11.970 m
f) Dist. waterline ballast to manifold	16.300 m
g) Dist. 1 <sup>st</sup> stander to manifold	0.54 m

\* without reducer

#### PARALLEL BODY LENGTH LOADED CONDITION

